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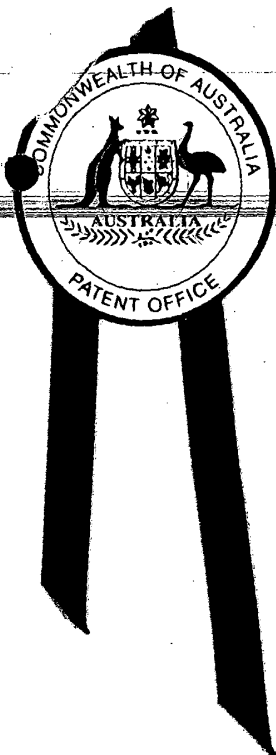
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*L. Myntt*  
LEANNE MYNOTT  
TEAM LEADER EXAMINATION  
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**ORIGINAL**

**PROVISIONAL SPECIFICATION**

**BIOXIDATION PROCESS AND APPARATUS**

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**The invention is described in the following statement:**

## BIOOXIDATION PROCESS AND APPARATUS

### Field of the Invention

This invention relates to biooxidation processes and reactors for the liberation of metals from minerals, especially sulphides, containing them.

### 5 Background to the Invention

Metal containing minerals, especially metal sulphides, may be oxidised using specific types of micro organism, especially bacteria in a bioextraction process. Oxidation of sulphide minerals may be used to put the metals into solution, from for example iron, copper, zinc, nickel and cobalt sulphides, or to  
10 release precious metals, such as gold, silver and platinum, encapsulated in metal sulphides, particularly in refractory ores. The process is known as bacterial oxidation, bioextraction, biooxidation, bioleaching, or bacterial leaching. In this respect pyrite, an iron sulphide, and arsenopyrite, an iron-arsenic sulphide are the most common minerals occluding gold in the so-called  
15 refractory gold ores and treatment of such materials by microorganisms may therefore assist in liberation of precious metals from refractory ores containing them.

Certain kinds of bacteria used in such processes have been documented and include the mesophiles, *Thiobacillus ferrooxidans*, *Thiobacillus thiooxidans*,  
20 *Leptospirillum ferrooxidans*, moderate thermophiles, and thermophiles such as *Sulpholobus*.

The above processes are the object of an extensive literature encompassing papers and patents. However, conventional methods of bacterial oxidation involve oxidation in agitated stirred tanks into which air is  
25 introduced or in heaps using rocks with a size of 6mm or greater in which fine particles may have been agglomerated or heaps using pelletised fine material. An acidic bacteria containing liquor is developed and typically used to irrigate the heap and facilitate metal extraction. The heap leaching technique has been used for many years and Brierley et al have patented a process (US Patent No.  
30 5246486) for a two stage agglomeration process for the recovery of gold from sulphide minerals in heaps where the mineral particles are of large size and not slurried.

Van Aswegen in the article "The Genmin Experience", has described bacterial oxidation in tanks made of stainless steel or other lined steel which contain a slurry of concentrate and water. The tanks are typically 9 metres high and 9 metres diameter and agitated with axial flow impellers which are driven by  
5 large motors. Compressed air is piped into the tank and sheared by the impellers into a fine dispersion of bubbles to maintain a desired dissolved oxygen concentration in the slurry. A variety of impellor types other than axial flow may be used such as turbines.

The present applicant has found that such methods suffer from a number  
10 of disadvantages. Primary among these is the high power consumption and high capital cost encountered in employing bacterial oxidation reactors agitated by impellers.

Although proposals have been made to employ diffusion means to maintain particles in suspension, notably in Envirotech US Patent Nos 4728082,  
15 4732608, 4968008, 4974816 and 5007620, it is uniformly recognised that there is a need to provide some mechanical means, for example in the form of a rake to ensure that significant quantities of solids are not deposited on the floor of the reactor vessel, reducing reactor efficiency.

### **Summary of the Invention**

20 It is the object of the present invention to provide an improved method and apparatus for carrying out bacterial oxidation especially of metal sulphide minerals.

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With this object in view, the present invention provides, in its first aspect, a process for recovering metals from materials containing them by biooxidation  
25 including treating, in a reactor, a slurry containing a metal containing material with bacteria capable of promoting extraction of metals from said metal containing material; and maintaining said material in suspension and bacterial viability in the reactor by introducing gas to the slurry within the reactor by aeration means.

30 The aeration means advantageously introduces gases to the reactor in the form of bubbles of controlled size, generally of small diameter to enhance mass transfer of oxygen to bacteria. It will be understood, in this respect, that the

bacterial oxygen demand is extremely high and oxygen diffusion characteristics important. Control of bubble size by shearing is not employed.

Suitable aeration/agitation means may particularly and advantageously include diffusers as described hereinbelow. Diffusers are devices that will both  
 5 introduce air or other gases to the slurry by diffusion mass transfer of gas from fine bubbles- advantageously of controlled size-to the solution or slurry and maintain solids in suspension for bacterial oxidation. Dome, tubular, disc or doughnut type diffusers may appropriately be used in accordance with the invention.

10 Aeration means may include hydraulic shear devices. In such devices, very fine bubbles are formed by dislodgment thereof before full development under the influence of shear forces.

Surface aerators such as paddle aerators may be used to break liquid surface and assist in entrainment of gas such as air in the bulk reaction slurry.

15 Reactor configuration may be varied to maximise aeration.

A further alternative would be the use of liquid jets where a stream of liquid from a reactor is pumped through a venturi which draws air into the liquid thereby aerating it. The aerated liquid is returned to the reactor.

In a particularly preferred embodiment, a gas appropriate for  
 20 maintenance of bacterial viability include oxygen containing gases, in particular air, oxygen enriched air or oxygen; optionally, with addition of carbon dioxide, such as air enriched with carbon dioxide, may be introduced to the aqueous  


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 solution by aeration means, particularly diffusers.

Where a biooxidation process is involved, various chemolithotrophic  
 25 bacteria may be employed. Various categories of bacteria may be employed in these processes. These categories are as follows:

- 1) mesophiles which are suitable for oxidation in the range 10°C to 45°C;
- 2) moderate thermophiles, which oxidise the sulphide minerals in the  
 30 range 40°C to 60°C; and
- 3) thermophiles which oxidise from above 50°C to 90°C.

The process may be carried out employing any one or more such

microorganisms, especially bacterial species, often referred to as a single or mixed culture respectively, which will oxidise sulphides or other minerals or metal containing materials in the required temperature range. Preferred mesophiles for use in bacterial oxidation are *Thiobacillus ferrooxidans*,  
 5 *Thiobacillus thiooxidans* and *Leptospirillum ferrooxidans*. Most of the moderate thermophiles do not have specific names, but some have been referred to as *Sulphobacillus thermooxidans*. Preferably, the thermophilic bacteria will be of the type *Sulpholobus brierleyi*, *Sulpholobus BC*, and *Sulpholobus acidocaldarius*. Notwithstanding naming of species herein, similar iron and  
 10 sulphur oxidising bacteria within the overall temperature range of 0°C to 90°C identified but not yet named are included within the scope of the present invention. The process is most advantageously conducted generally in the temperature ranges for which the bacteria are tolerant as described above. Reaction may be undertaken in the mesophilic, moderately thermophilic or  
 15 extreme thermophilic temperature range.

Though the process may be employed exclusively for metal liberation, pre or post treatment by other metallurgical operations, such as CIP or CIL processes for recovery of precious metals for example, may be employed where desirable. Solid/liquid separation may typically follow biooxidation, liquor being  
 20 further treated for metal recovery.

The process may be conducted in any suitable reactor, including those types of reactor already generally known to the art, operating advantageously  
 on a continuous basis. Aeration may be achieved by including, in such reactors, suitable aeration means even in large capacity systems.

25 However, it is intended that no mechanical means be employed within the reactor, that the introduction of gas be employed as the sole agency by which particles are maintained in suspension without significant build-up of mineral containing particles constituting the metal containing material on the floor of the reactor. Such a reactor may be said to be rakeless.

30 In a particularly preferred embodiment, the metal containing material is, for example, a non-ferrous base metal sulphide ore, such as a copper, nickel, zinc, lead or cobalt containing ore, including mixed or polymetallic ores, or a

refractory gold ore incorporating occluding sulphides amenable to dissolution by bacterial action. Other materials in this class may include flotation concentrates, gravity concentrates, tailings, precipitates, mattes and sulphidic fume. However, the above process is also suitable for carrying out bacterial  
5 oxidation and bioleaching of non-sulphide ores and other generally inorganic materials containing metals in economic concentrations, where suitable bacteria are available to carry out the process. For example, without intending to limit the invention in any way, bioleaching of rare earth ores, oxidic manganese ores and phosphate rock is possible in accordance with process of the invention.

10 In a further embodiment of the invention, there is provided a reactor system for biooxidation treatment of metal containing materials including at least one rakeless reactor having a reaction volume provided with aeration means for introducing gas for maintaining said metal containing material in suspension and bacterial viability.

15 The reactor may take various forms, though incorporates no mechanical means of agitating the reactor volume, and may for example be in the form of tanks or vats. In this case, the reactor may be fabricated from suitable materials, steel, metal alloys or concrete optionally lined with an acid resistant medium. Additional materials of construction include wood, plastic, fibre-glass or any  
20 suitable aeration means may be as known in the art.

Alternatively, a reactor may take a reservoir configuration being formed by excavation above or below ground. In such a case, the reservoir may be  
lined with a liquid impermeable barrier, such as clay or plastic membrane, to prevent solution entering the surrounding ground or rock. The reactor may be  
25 built from rock or other suitable material above the surrounding ground surface.

In a reservoir configuration, though the following may be applicable to other types of suitable reactor, the reactor is preferably rectangular in plan section. The reactor may be tapered towards either end. When viewed from an end the reactor may also be rectangular in section though other shapes may be  
30 employed. The walls of the reactor may be substantially vertical or sloped. The depth of the reactor may typically be between 4 and 8 metres, and the width between 5 and 20 metres though both dimensions could be larger or smaller.

Very large reactors, possibly having length greater than 100 metres, may be built and a number of reactors may be employed. Such reactor systems may be combined in series or operated in parallel.

The bottom of the reactor may be sloped so that there is a gradient from the feed end at which ore or other metal containing material is fed into the reactor to the discharge end. This slope may be a descending slope. The gradient of the reactor may be variable. This may assist in transfer of particles from feed to discharge. Volume of the reactor is calculated in dependence upon the rate at which the metal containing material or mineral is being treated.

Feed may be introduced at one end of the reactor through multiple points located along the width of one end. Distribution of slurry to these points may be via a ring main or splitter of conventional type.

However, it is not intended to restrict possible reactor designs to the above configurations and other configurations could be employed.

#### 15 **Brief Description of the Drawings**

Description of preferred embodiments of the invention now follows. The description is made with reference to the accompanying drawings in which:

Figure 1 is a side sectional view of an aeration means to be used in accordance with a first embodiment of the process of the present invention;

Figure 2 is a plan view of the aeration means shown in side section in Figure 1;

Figure 3 is a side sectional view of an aeration means to be used in accordance with a second embodiment of the process of the present invention;

Figure 4 is a plan view of the aeration means shown in side section in Figure 3;

Figure 5 is a schematic diagram showing flow circulation in a reactor, including a tubular aeration means, as operated in accordance with a third embodiment of the process of the present invention;

Figure 6 is a schematic diagram showing flow circulation in a reactor including disc aeration means, as operated in accordance with a fourth embodiment of the process of the present invention.

Referring specifically to the Figures 1 to 4, the gas is delivered through



diffusers, i.e a means for diffusing a gas into the liquid portion of a slurry or solution. Typically, compressed air - though other gases as described above may be suitable - is blown through gas supply line 10 to the diffuser unit 1 passing through a perforated wall 11 thereof forming air bubbles which serve to transfer oxygen and carbon dioxide into a slurry 2 in a reactor (not shown) for bacterial respiration and for oxidation of minerals. Gas supply line 10 may service a number of reactors. A slug flow introduction of air or gas to the reactor, that is, without control over bubble size at introduction to the reactor, is not desirable and is, most advantageously, to be avoided.

10 Diameter or size of the perforations 13 in wall 11 dictates bubble size, if desired, in a controlled manner. The smaller the bubble size the greater the surface area per unit of volume providing efficiency of gas-liquid contact allowing the high values of oxygen transfer that are necessary for efficient bacterial oxidation. Bubble size is to be maintained at 7.5mm average diameter  
15 or less, preferably 5mm average diameter or less.

Disc, doughnut or tubular designs may be employed, the first two types being shown in Figures 1 to 4.

A disc diffuser, as seen in side section in Figure 1 and plan in Figure 2, is manufactured from a flexible membrane 15 that closes when no air is being  
20 delivered. This ensures that no slurry enters gas supply line 10 during processing. The membrane 15 may be retained in position by a retaining device such as a clamping ring 16 which fixes the membrane in position 15  
about an outlet 20 of the gas supply line 10. As the membrane 15 expands with  
air flow, perforations in the form of pores in the membrane open allowing air flow  
25 therethrough. The pores 13 may advantageously be microscopic, of the order of 1 to 5 $\mu$  in diameter. As a result, impellor action is not required to shear air slugs to an appropriate bubble size distribution to optimum transfer of oxygen to the slurry. Further the mass transfer occurs in a readily controllable fashion and the bubble size may be controlled by selecting a membrane or other material (see  
30 below) with desired pore or hole size.

A doughnut shaped diffuser is shown in side section in Figure 3 and plan in Figure 4. Again, a membrane 15 is employed which has the same

characteristics as discussed above. However, here the gas supply line 10 serves further supply lines 23 feeding the doughnut shaped tube 24, the walls of which are formed from membrane 15 thereby providing greater contact area of membrane 15 with solution or slurry.

5 Characteristics of membrane 15 may include flexibility, relatively low cost, durability and easy replacement. The membrane 15 may be formed from acid resistant rubber or other polymers with a pore size distribution as desired for use in the process. The membrane may be manufactured in a known manner in the field of membrane technology.

10 A further type of diffuser is of typically dome shape and manufactured from plastics or ceramics. The material is perforated with holes of similar diameter to that above that are fixed and open all the time allowing air to flow therethrough to form a bubble swarm in the slurry within the reactor.

A particularly effective type of diffuser is tubular with the tubular body 15 perforated with holes for gas exit preferably having a U-shaped configuration. The tubular body may be connected to the gas supply line and may be formed from a membrane or suitable plastic or ceramic material.

Diffusers suitable for the application will typically be sized to allow a sufficient volume of gas to be diffused into the slurry to achieve between 0.5 and 20 15 mg/l dissolved oxygen concentration in the slurry depending upon the oxygen requirement of the bacteria used in the biooxidation process. There may be provided a number of diffusers as necessary to maintain solids in suspension and supply sufficient gas for oxidation.

Reactor configuration may be selected to achieve optimal aeration. 25 Diffuser(s) may be placed at, or just off, the base of the reactor, if applicable, spaced at intervals - possibly with different rates of gas introduction - to give a suitable bubble distribution for the material being treated. The diffusers are fixed in position. Under different circumstances, the number of diffusers required to maintain the solids in suspension may be greater than that required 30 for oxidation, at other times the number required may be lower. A uniform arrangement throughout the reactor base may be preferred. Conveniently, the number of aeration means or diffusers per unit area within the reactor may vary

such that there is a greater proportion at the feed end of the reactor where higher rates of bacterial oxidation would be expected than at the discharge end.

Figures 5 and 6 show, without intending to limit the invention, likely flow circulation patterns for a number of tubular and disc diffusers located in a reactor  
5 100. It may be understood that each arrangement allows efficient mixing and bacterial/solid contacting though a disc diffuser arrangement may be preferred.

Diffusers may also be provided in pipelines connecting the reactor with others in the reactor system. Alternatively, gas may be introduced at these points by other suitable means. This may be especially applicable in the case of  
10 a heap or dump leaching process in which ore particles are not placed into suspension in the leach liquor.

Materials treated by the process and reactor systems of the invention may include ores, concentrates obtained from ores, tailings, wastes and other materials having sufficient metal values present to economically remove the  
15 metal or to remove metals detrimental to the environment or other processes. It is to be understood that the present invention is not limited to the treatment of sulphides.

The metal value containing material may require to be pre-treated, for example crushed, to a size sufficiently small to enable it to be ground in  
20 conventional comminution equipment such as ball mills.

Conveniently, the solids requiring oxidation are ground to a particle size ~~sufficiently fine for the gas to be effectively used in maintaining a suspension~~ thereof and without allowing significant build-up on the floor of the reactor. Typically, grinding to a particle size distribution necessary to meet this criterion.  
25 The size of the product after grinding is preferably 90% passing 50 microns or less. It is advantageous for the ore or other metal containing material to be ground in an ultra fine grinding machine to particle size between 80% passing 2 microns and 80% passing 30 microns in accordance with a further embodiment of the invention. The bottom particle size is as small a size as is practically  
30 attainable by grinding. The size of the particles should be chosen to be the optimum for maintaining the solids in suspension and carrying out a bacterial oxidation process.

Conveniently, after crushing and/or grinding the material concentration may occur by gravity, flotation or other beneficiation processes to increase the proportion of the sulphides or other desired minerals in the product. However, the process is equally applicable to the treatment of concentrates of residue  
5 produced by others and comminution pre-treatment is not necessarily required in each case.

The ground metal containing ore or concentrate is preferably slurried with an aqueous solution, especially water. Slurries from grinding may be diluted within additional water and pumped into the reaction zone in which the  
10 biooxidation process is to take place. The pulp density of the slurry introduced to the reactor of the invention may be of great importance to the attainment of the objection of the invention, accordingly a range of 5 to 15% or upward may be selected. At lower pulp density, as stated, efficient bacterial activity may be achieved as toxic effects due to high ionic concentration; and/or mechanical  
15 grinding of bacteria are avoided. Leaching is enhanced by the very low shear, low ionic concentration environment. Bacteria are ideally previously added to the reactor in the form of a culture with a mineral and grown in sufficient numbers so that there are preferably between  $10^5$  and  $10^9$  bacteria per millilitre of slurry. The bacteria may be maintained in the reactor according to accepted  
20 practice or by a method of immobilisation.

Preferably the retention time in the reactor is 2 to 8 days. The retention time may be longer to allow treatment of less finely ground material, which  

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requires a longer time to be processed, or to achieve higher levels of mineral oxidation and dissolution of the metal. The amount of gas introduced to the  
25 slurry may be changed in accordance with retention time but this is not essential.

Conveniently, the bacterial oxidation process is carried out in an acidic solution which is suitable for growth of the specific bacteria, for example thiobacilli, used. This is expected to be in the range of 0.5 to 3.0. Preferably, the  
30 pH will be in the range 0.8 to 2.5. An initial acid addition may be required at the start of the process to neutralise acid consuming minerals and maintain the pH in the required range. The process of oxidising sulphide minerals produces

acidic by-products and it is likely that the pH will decrease during processing. If necessary, the pH may be maintained in the required range by controlled addition of a base or basic agent such as lime, limestone or any other suitable alkali.

- 5       Where the material to be treated is not a sulphide, reaction may be carried out under alkaline conditions. In these situations the pH is to be kept at a level suitable to the specific leaching conditions.

Support of the bacteria is likely to require the addition of nutrients to maintain growth. Typical nutrients to be introduced to the reaction zone are  
10   nitrogen, sulphur and phosphorus containing materials such as ammonium sulphate, potassium dithiophosphate and magnesium sulphate. In addition, other nutrients may be required for specific ores and concentrates as is known in the art.

Further, as oxidation of sulphide minerals is an exothermic process, heat  
15   will be released during bacterial oxidation. This may be a problem where ores are treated but may be especially true where an enriched sulphide concentrate is treated. In this case, the release of heat may increase the temperature of the slurry in the reactor above that tolerated by the bacteria, especially thiobacilli. Sulpholobus bacteria are more temperature tolerant. Therefore, the reactors

- 20   are typically to be provided with cooling systems. Water may be a suitable coolant and the cooling system may be direct, with coolant water introduced at the base of the reactor. Alternatively, indirect cooling may be employed using conventional heat exchanger technology. For example, a cooling tower could produce cold water which feeds cooling coils, tube bundles or like means  
25   suitably located in the reactor. Tube bundles and coils may be preferred in the absence of strong currents generated by stirring or agitation by turbine blades. Evaporative cooling may be promoted by reducing depth of a reservoir and increasing the surface area. The coolant may be introduced at sufficient velocity to assist in maintaining solids in suspension and admitted water may counteract  
30   evaporation losses.

More generally, a temperature control system with heating/cooling functions may be employed. The location and nature of temperature control

system, internal or external, direct or indirect, may be varied to achieve the required temperature control of the reactor. For example, when thermophilic bacteria are used, heating to above 60°C may be required.

Other uses of the process may be exemplified, without limitation, as follows:

#### **Ferric Ion Generation**

The process of the invention is suitable for converting ferrous ions in solution to ferric ions which may attack minerals, for example uranium minerals, to liberate metal values of economic interest.

#### **Treatment of Manganese Containing Ores**

Manganese ores may be treated by mixing with a metal sulphide with the parameters for bacterial oxidation being as above described.

Alternatively, manganese ores may be bioleached with the organism *Enterobacter* at pH controlled between 4 and 8.

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#### **Sulphur Removal from Coal**

The mineral pyrite occurs with coal and bacterial oxidation using chemolithotrophic bacteria has been used to remove pyrite and reduce sulphur content. The process of the invention may be employed for sulphur removal

20 with the parameters for bacterial oxidation being as above described.

In accordance with the process and reactor systems of the invention the grade of ore, concentrate or other metal containing material may be lower than that for agitated tanks and like reactor systems because of expected lower capital and operating costs.

5 The invention will be more fully understood from the description of the following examples.

#### **Example A      Inert Material**

A trial was conducted on an inert mineral used to duplicate sulphide ores and concentrates.

10 A 10% weight percent slurry with a sizing of 90% passing 16 micrometers

was maintained in uniform suspension in a tank with fine air bubbles injected from a close packed array of commercially available membrane diffusers at the base of a 1.4 metre diameter by 4 metre high tank. The height of tank is similar to that used in commercial practice.

- 5 Air flows of at least 2.4 Nm<sup>3</sup>/h/diffuser was required to prevent settling of solids. The air flow rates required were within the manufacturer's recommended operating range.

Solids that settled because of a reduction or disruption in air flow were re-suspended when the air flow was re-established at 2.4 Nm<sup>3</sup>/h/diffuser or higher.

- 10 These results showed that a typical ground sulphide concentrate with a sizing of 90% passing 12 micrometres would stay in suspension under the same operating conditions.

The operating conditions with respect to air flow were set to duplicate an oxygen demand of 1.5 kilograms per cubic metre hour which is equivalent to  
15 that required for bacterial oxidation of sulphide minerals.

#### **Example B      Leaching of Refractory Gold Sulphide Concentrate**

A sample of gold concentrate containing arsenopyrite and pyrite was ground to a size such that 80% of the particles were less than 15 micrometers in diameter.

- 20 The biooxidation reactor, constructed from conventional acid resistant material, had a volume of 200 litres and was provided, at its base, with a membrane diffuser as described in Example A. Air was supplied to the diffuser at a rate which maintained the ground solids in suspension. No other agitation was used.

- 25 The ground concentrate was mixed with water to produce a slurry at 10% solids on a weight to volume basis. Sulphuric acid was added to the slurry to obtain an acidity level of pH 1.2. Approximately five litres of an inoculum slurry containing a mixture of mineral concentrate and moderately thermophilic bacteria was added to the slurry in the reactor. Thereafter a mixture of nutrients  
30 comprising hydrated magnesium sulphate, potassium orthophosphate, and

ammonium sulphate was added to the slurry.

The reactor was then heated such that the temperature of the slurry was maintained at 48°C, in the moderate thermophile range.

Air was added to the reactor from a standard compressor, through a flowmeter with a flow valve and thence into a pipe connected to the diffuser.

The air flowrate was controlled to allow a steady stream of bubbles to be emitted from the diffuser. The air was used to maintain the particles in suspension and also to supply the oxygen requirement of the bacterial culture.

No additional agitation of the reactor volume was employed. Samples of the slurry were taken on a daily basis to determine the extent of oxidation of the arsenopyrite/pyrite concentrate.

	Time (days)	Oxidation Level (%)	
		Arsenic	Iron
15	6	100	na
	32	100	94

The final residue in the tank was analysed after the test had proceeded for 32 days.

	Assay (wt%)		
	As	Fe	S <sup>2-</sup>
Initial Concentrate	3.05	21.0	23.0
Final Residue	0.03	0.4	0.1
Oxidation (%)	99	96	99

S<sup>2-</sup> is the amount of sulphide sulphur present and determines the amount of total oxidation that has occurred. Based on the analysis of the residue, the oxidation extent was determined.

Gold was then extracted from the residue using conventional cyanide leaching. The residue assayed 67 g/t gold of which 99% was extracted by cyanidation.



### Example C      Leaching of Copper Concentrate

A sample of copper concentrate containing chalcopyrite (and designated "CP1") was ground to a size such that 80% of the particles were less than 10 micrometers in diameter.

- 5      Again, the biooxidation reactor had a maximum volume of 200 litres and a membrane diffuser, as described in Example A, was installed at the base. Air was supplied at a rate to maintain the ground solids in suspension and maintain oxygen requirement of the bacteria. No other agitation was employed.

- 10      The ground concentrate was mixed with water to produce a slurry at 5% solids on a weight to volume basis. Sulphuric acid was added to the slurry to obtain an acidity level of pH 1.2. Approximately 5 litres of an inoculum slurry containing a mixture of mineral concentrate and moderately thermophilic bacteria was added to the slurry in the reactor. Thereafter, a mixture of nutrients comprising hydrated magnesium sulphate, potassium orthophosphate, and  
15 ammonium sulphate was added to the slurry.

The reactor was then placed in a heated room such that the temperature of the slurry was maintained at 48°C.

Air was introduced to the reactor from a standard compressor, through a flowmeter with a flow valve and thence into a pipe connected to the diffuser.

- 20      The air flowrate was controlled to allow a steady stream of bubbles to be emitted from the diffuser. The air was used to maintain the particles in suspension and provide the oxygen requirement of the bacteria. No additional agitation of the reactor was employed. Samples of the slurry were taken on a daily basis to determine the extent of oxidation of the arsenopyrite/pyrite  
25 concentrate.

	Conditions	CP1
Copper Content (%)		18
Copper Extraction (%)	Acid Leach only	4
Copper Extraction (%)	Bacterial oxidation leach	
5	using moderate thermophilic bacteria	84

### **Example D      Polymetallic Concentrate**

#### **D.1    Leaching with Mesophilic Bacteria**

In this example, the reactor used was 125mm diameter and 1.7m high. A synthetic rubber diffuser was installed in the base of the reactor.

10      A sample of mixed polymetallic concentrate (designated "M1") containing a mixture of mineral sulphides was biooxidised to extract zinc, nickel, copper and cobalt. The concentrate contained the nickel mineral pentlandite, as well as nickel contained within the structure of the mineral pyrrhotite. Copper was predominately present in the form of chalcopyrite though chalcocite and bornite  
15 were also present. Zinc was present as sphalerite. The metal cobalt was associated with the nickel minerals and as the mineral cobalt. The concentrate was ground to a size such that 80% of the particles were less than 15 micrometers in diameter.

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The ground concentrate was mixed with water to produce a slurry at 10%  
20 solids on a weight to volume basis. Sulphuric acid was added to the slurry to obtain an acidity level of pH 1.2. Approximately half a litre of an inoculum slurry containing a mixture of mineral concentrate and mesophilic bacteria (*Thiobacillus ferrooxidans* and *Thiobacillus thiooxidans*) was added to the slurry in the reactor. Thereafter, a mixture of nutrients comprising hydrated  
25 magnesium sulphate, potassium orthophosphate, and ammonium sulphate was added to the slurry.

The reactor was then placed in a heated room such that the slurry temperature was maintained at 35°C.

Air was introduced to the reactor from a standard compressor, through a

flowmeter with a flow valve and thence into a pipe connected to the diffuser.

The air flowrate was controlled to allow a steady stream of bubbles to be emitted from the diffuser. The air was used to maintain the particles in suspension and to supply the oxygen requirement of the bacteria. No additional  
5 agitation of the reactor was employed. The concentrate was oxidised with metals being released into solution. The level of extraction of the metals was determined by analysing a portion of the liquid fraction of the slurry. When the reaction was complete, the solid and the liquid phases were separated and the solution and the solids analysed.

10	Conditions	M1
	Copper Content (%)	5.7
	Nickel Content (%)	0.9
	Cobalt Content (%)	0.06
	Zinc Content (%)	0.21
15	Sulphur Oxidation (%)	98
	Copper Extraction (%)	Bacterial oxidation leach 92
	Nickel Extraction (%)	using thermotolerant bacteria 97
	Cobalt Extraction (%)	97
	Zinc Extraction (%)	95

## 20 D.2 Leaching with Moderate Thermophiles

~~In this example, the reactor used was 125mm diameter and 1.7m high. A~~  
synthetic rubber diffuser was installed in the base of the reactor.

A sample of mixed polymetallic concentrate (designated "M2") containing a mixture of mineral sulphides was biooxidised to extract zinc, nickel, copper  
25 and cobalt. The concentrate contained the nickel mineral pentlandite, as well as nickel contained within the mineral pyrrhotite. Copper was predominately present in the form of chalcopyrite though chalcocite and bornite were also present. Zinc was present as sphalerite. The metal cobalt was associated with the nickel minerals and as the mineral cobalt. The concentrate was ground to a  
30 size such that 80% of the particles were less than 15 micrometers in diameter.

The ground concentrate was mixed with water to produce a slurry at 10%

solids on a weight to volume basis. Sulphuric acid was added to the slurry to obtain an acidity level of pH 1.2. Approximately half a litre of an inoculum slurry containing a mixture of mineral concentrate and moderately thermophilic bacteria (*Thiobacillus ferrooxidans* and *Thiobacillus thiooxidans*) was added to the slurry in the reactor. Thereafter, a mixture of nutrients comprising hydrated magnesium sulphate, potassium orthophosphate, and ammonium sulphate was added to the slurry.

The reactor was then placed in a heated room such that the slurry temperature was maintained at 47°C.

10 Air was introduced to the reactor from a standard compressor, through a flowmeter with a flow valve and thence into a pipe connected to the diffuser.

The air flowrate was controlled to allow a steady stream of bubbles to be emitted from the diffuser. The air was used to maintain the particles in suspension and to supply the oxygen requirement of the bacteria. No additional agitation of the reactor was employed. The concentrate was oxidised with metals being released into solution. The level of extraction of the metals was determined by analysing a portion of the liquid fraction of the slurry. When the reaction was complete, the solid and the liquid phases were separated and the solution and the solids analysed.

20	Conditions	M2
Copper Content (%)		7.3
Nickel Content (%)		0.8
Cobalt Content (%)		0.05
Zinc Content (%)		0.24
25 Sulphur Oxidation (%)		77
Copper Extraction (%)	Acid leach only	12
Nickel Extraction (%)		10
Cobalt Extraction (%)		13
Zinc Extraction (%)		24
30 Copper Extraction (%)	Bacterial oxidation leach	93
Nickel Extraction (%)	using thermotolerant bacteria	98
Cobalt Extraction (%)		97
Zinc Extraction (%)		96

### D.3 Leaching with Thermophiles

In this example, the biooxidation reactor was of 40mm diameter and 1.0m height. A sintered diffuser was installed in the base of the reactor.

A sample of mixed polymetallic concentrate (designated "M3") containing  
5 a mixture of mineral sulphides was biooxidised to extract zinc, nickel, copper and cobalt. The concentrate contained the nickel mineral pentlandite, as well as nickel contained within the mineral pyrrhotite. Copper was predominately present in the form of chalcopyrite though chalcocite and bornite were also present. Zinc was present as sphalerite. The metal cobalt was associated with  
10 the nickel minerals and as the mineral cobalt. The concentrate was ground to a size such that 80% of the particles were less than 15 micrometers in diameter.

The ground concentrate was mixed with water to produce a slurry at 3% solids on a weight to volume basis. Sulphuric acid was added to the slurry to obtain an acidity level of pH 1.2. Approximately 100ml of an inoculum slurry  
15 containing a mixture of mineral concentrate and thermophilic bacteria (*Sulpholobus*) was added to the slurry in the reactor. Thereafter, a mixture of nutrients comprising hydrated magnesium sulphate, potassium orthophosphate, and ammonium sulphate was added to the slurry.

The reactor was then heated such that the slurry temperature was  
20 maintained at 70°C.

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Air was introduced to the reactor from a standard compressor, through a flowmeter with a flow valve and thence into a pipe connected to the diffuser.

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The air flowrate was controlled to allow a steady stream of bubbles to be emitted from the diffuser. The air was used to maintain the particles in  
25 suspension and to supply the oxygen requirement of the bacteria. No additional agitation of the reactor was employed. The concentrate was oxidised with metals being released into solution. The level of extraction of the metals was determined by analysing a portion of the liquid fraction of the slurry. When the reaction was complete, the solid and the liquid phases were separated and the  
30 solution and the solids analysed.

	Conditions	M2
	Copper Content (%)	5.0
	Nickel Content (%)	0.78
	Cobalt Content (%)	0.07
5	Zinc Content (%)	0.67
	Sulphur Oxidation (%)	84
	Copper Extraction (%)	Bacterial oxidation leach 99
	Nickel Extraction (%)	using thermotolerant bacteria 100
	Cobalt Extraction (%)	98
10	Zinc Extraction (%)	97

### Example E      Zinc Concentrate

In this example, the biooxidation reactor was of 40mm diameter and 1.0m height. A sintered diffuser was installed in the base of the reactor.

A sample of zinc concentrate (designated "Z1") containing a mixture of mineral sulphides was treated to extract zinc. The concentrate contained the zinc as the mineral sphalerite. The sample also contained lead sulphide as galena. The concentrate was ground to a size such that 80% of the particles were less than 15 micrometers in diameter.

The ground concentrate was mixed with water to produce a slurry at 5% solids on a weight to volume basis. Sulphuric acid was added to the slurry to obtain an acidity level of pH 1.2. Approximately 100ml of an inoculum slurry containing a mixture of mineral concentrate and moderately thermophilic bacteria (*Thiobacillus ferrooxidans* and *Thiobacillus thiooxidans*) was added to the slurry in the reactor. Thereafter, a mixture of nutrients comprising hydrated magnesium sulphate, potassium orthophosphate, and ammonium sulphate was added to the slurry.

The reactor was then heated such that the slurry temperature was maintained at 48°C.

Air was introduced to the reactor from a standard compressor, through a flowmeter with a flow valve and thence into a pipe connected to the diffuser.

The air flowrate was controlled to allow a steady stream of bubbles to be emitted from the diffuser. The air was used to maintain the particles in suspension and to supply the oxygen requirement of the bacteria. No additional

agitation of the reactor was employed. The concentrate was oxidised with zinc being released into solution. The level of extraction of the zinc was determined by analysing a portion of the liquid fraction of the slurry.

Conditions		Z1
5	Zinc Content (%)	25
	Sulphur Oxidation (%)	60
	Zinc Extraction (%)	
	Bacterial oxidation leach	
	using moderate thermophilic bacteria	97

#### 10 Example F      Ferrous to Ferric Conversion

A further test was carried out in a reactor which was 25mm diameter and 1.0m high. A sintered diffuser was installed in the base of the reactor.

A sample of ferrous sulphate was added to the reactor and diluted with water to obtain a strength of 9 g/l iron. Sulphuric acid was added to the slurry in the reactor to obtain an acidity level of pH 1.2. Extremely thermophilic bacteria (*Sulpholobus*), extracted onto a filter paper to separate them from other residual solution, were added to the slurry in the reactor. Thereafter, a mixture of nutrients comprising hydrated magnesium sulphate, potassium orthophosphate, and ammonium sulphate was added to the slurry.

20      The reactor was then heated such that the solution temperature was maintained at 70°C.

Air was introduced to the reactor from a standard compressor, through a flowmeter with a flow valve and thence into a pipe connected to the diffuser.

25      The air flowrate was controlled to allow a steady stream of bubbles to be emitted from the diffuser. The air was used to maintain the particles in suspension and to supply the oxygen requirement of the bacteria. No additional agitation of the reactor was employed.

The ferric solution was oxidised so that the ferrous ion was converted into ferric ion. The level of conversion of the ferrous ion was determined by titration

30

with potassium dichromate.

Modifications and variations may be made to the process and reactor system of the present disclosure without departing from the scope of the invention.

DATED this 18th day of NOVEMBER, 1998

<sup>P+1</sup>  
**BACTECH (AUSTRALIA) LIMITED**



WATERMARK PATENT & TRADEMARK  
ATTORNEYS

4TH FLOOR, "DURACK CENTRE"

263 ADELAIDE TERRACE

PERTH W.A. 6000

AUSTRALIA



Fig 1.

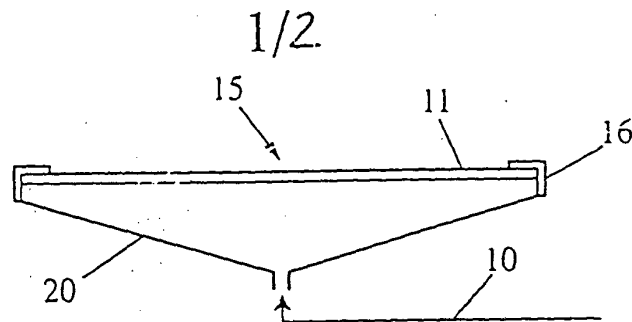


Fig 2.

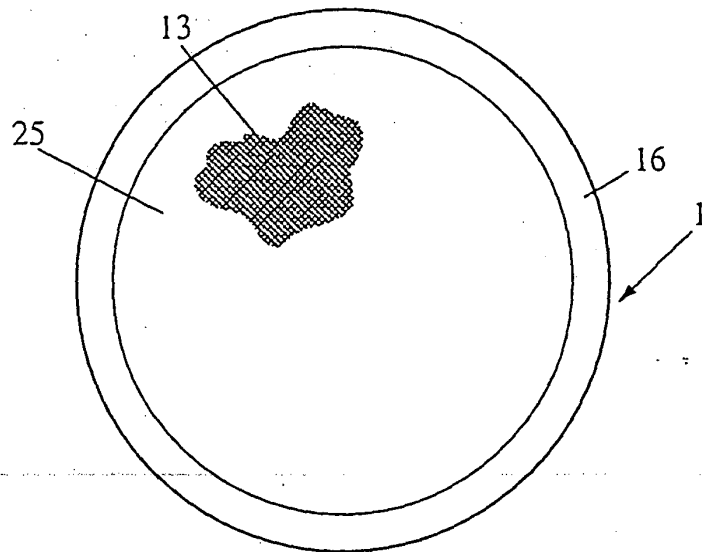


Fig 3.

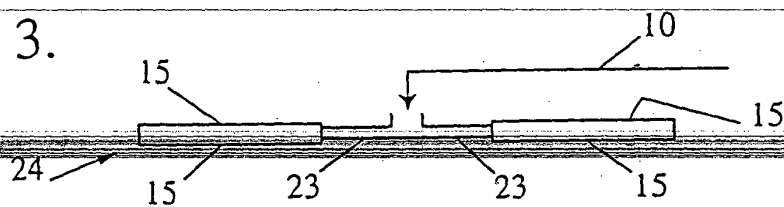
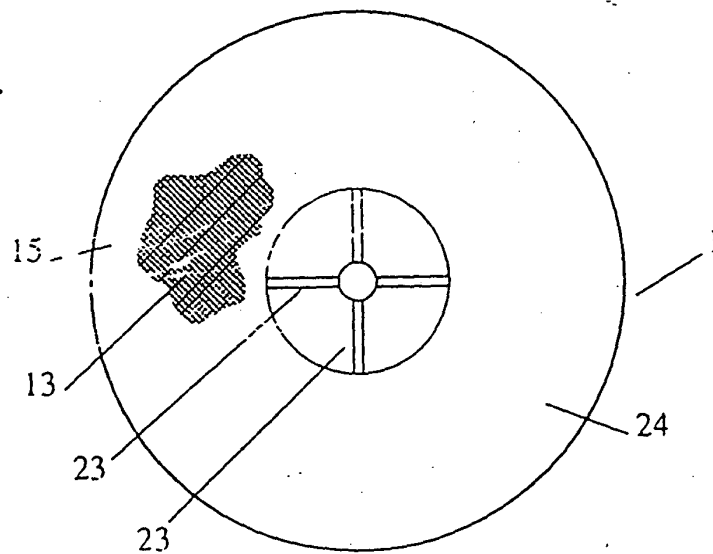
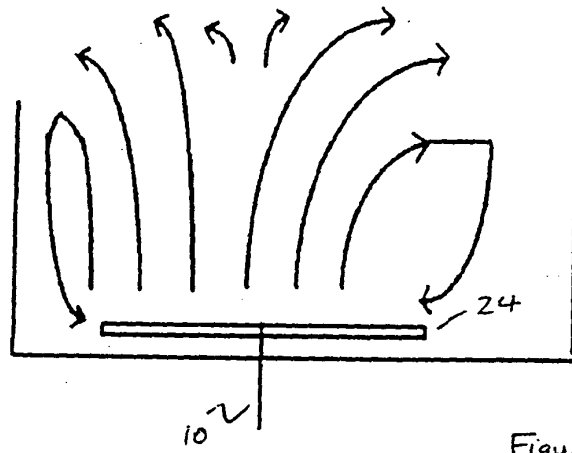


Fig 4.





Bubble Tube

Figure 5

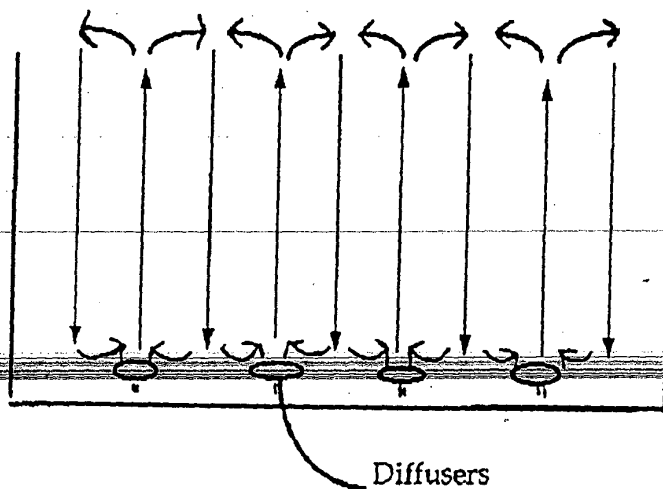


Figure 6



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